

# **CFD MODELLING TO RELATE GEOMETRIES AND COEFFICIENT DISCHARGE IN VENTURIMETER**

A DISSERTATION

MASTER OF TECHNOLOGY

IN

HYDRAULICS AND WATER RESOURCES ENGINEERING

BY

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**(2K19/HFE/12)**

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## ABSTRACT

Liquid stream qualities incorporate fluid, just as gas, assumes a fundamental part in the advanced designing ground having broad function in the businesses. The examination of liquid stream and its attributes is fundamental to execute testing with designing investigations. Calculation of stream pace during a line is finished with the distinction of pressing factor top accessible at the cross-segment space of the line. The gauge which plays out the said calculation of liquid stream named as a venturigauge. Venturigauge discovers valuable in plumbing, liquid oil pipeline, car carburetor, petrol synthetic enterprises, and so on In this trial study, an examination is completed in liquid designing lab outfitted with office for stream alignment. Venturigauge plus opening gauge are utilized to gauge release coadjuvants for the liquid measured in the trial. The effect of points on liquid qualities is concentrated by displaying through computational fluid elements advance Liquid stream inside venturigauge is simulate with a consistent stream in k-epsilon replica. The test replica got with the beta proportion 0.6 along with contributions of three distinct plots for joined just as a disparate part of venturi. The particular points are 21,20, 22 and 9,11,7 for focalized and different side, individually. Pre-handling of test replica calculation was executed utilizing CREO. In the preparing stage, ANSYS apparatus was used for the lattice and meaning of limit circumstances. Inside post-handling, forms of pressing factor and speed were resolved with CFX solver. The test information was approved and contrasted and CFXeffect.

## CERTIFICATE

I hereby certify that the project Dissertation titled “ **CFD Modelling To Relate Geometries And Coefficient Discharge In Venturimeter**” which is submitted by, Roll number **2K19/HFE/12** of M. Tech (HRE), Delhi Technological University, Delhi in the requirement for the award of the degree of Master of Technology, is record of the project carried out by the students under my supervision. To the best of my knowledge this work has not been submitted in part or fully for any Degree or Diploma To this University or elsewhere.



(Dr. BHARAT JHAMNANI)

(SUPERVISOR)

Place: Delhi

Date:

# Table of Contents

ACKNOWLEDGEMENT .....	1
ABSTRACT .....	2
CERTIFICATE .....	3
CHAPTER 1: INTRODUCTION .....	1
1.1 Venturimeter .....	4
1.2 CFD Techniques .....	7
1.3 Analysis of CFD Replicating .....	8
1.4 Problems of CFD Replicating .....	10
1.5 Ansys Fluent .....	10
1.6 Features of Ansys Fluent.....	11
1.6.1 Meshes, Numerics and Parallel Processing .....	11
1.6.2 Dynamic & Moving Mesh .....	12
1.6.3 Turbulence & Acoustics .....	12
1.6.4 Heat Transfer, Phase Change & Radiation .....	13
1.6.5 Reacting Flow .....	13
1.6.5 Multiphase.....	14
1.6.6 Post-Processing and Data Export.....	14
1.6.7 Customized Tools .....	15
1.7 Math and cross section .....	15
1.8 Objectives .....	16
CHAPTER 2 : REVIEW OF LITERATURE.....	18
CHAPTER 3 : MODELING AND ANALYSIS .....	31

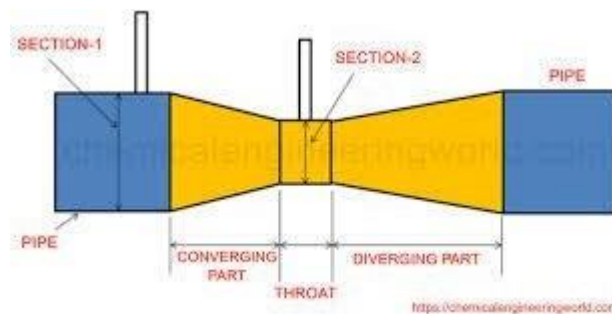
3.1 Type 1 .....	33
3.2 Geometry type 2.....	35
3.3 Geometry type: Three .....	37
<b>CHAPTER 4 : CONCLUSIONS AND DISCUSSIONS .....</b>	<b>44</b>
<b>REFERENCES .....</b>	<b>50</b>

## CHAPTER 1: INTRODUCTION

The venturi gauge is a deterrent gauge named to pay tribute to Giovanni Venturi, an Italian physicist who initially tried cone shaped developments and constrictions. The first, or old style, venturi was concocted by a U.S. wangle, Clemens Herschel, in 1898. It's anything but a 21-degree tapered withdrawal, a instantly gullet of breadth  $d$  and span  $d$ , then, at that point seven to fifteen degree cone shaped extension. The fundamental standard on which an endeavor gauge work is that by diminishing the crosssectional space of the stream section, a pressing factor distinction is made, and the estimation of this pressing factor contrast empowers the assurance of release through a line. These days, it is important to play out the alignment trial of the stream gauges to discover the precision of the gadget. These should be possible by computing the release coadjuvant of the venturi. Albeit test methodology present a decent outcome, they are frequently tedious. Henceforth a more complex strategy for testing the stream gauge is through mathematical strategies.

Because of an assortment of business CFD codes being accessible on the lookout, it is feasible to acquire more precise outcomes which require some investment. These outcomes can then measure up to the underlying trial results to align the instrument. Lines as liquid streams are broadly utilized in channeling frameworks in the business, removal, and circulation of drinking water. The arrangement of lines are planned so as to have the option to address the issue for liquid dissemination. Different sorts and points of line spreading in funneling frameworks will create diverse stream disseminations. Estimation of stream coursing throughout the shut conduit is finished by utilizing venturi gauges. The situation experienced in chunky fluid gaugeing can be past the extent of use for commerce guidelines. The venturi gauges have merged cone deltas, tube shaped necks, and different recuperation cones. It has no protrusion to the fluid; there is no prickly point and no abrupt transform in the form. The accompanying diagram one illustrate venturi gauge with identical tube shaped division prior to merging, collar waterway plus disparate.

Because of united passageway speed of liquid stream increments and pressing factor diminishes in chamber neck pressing factor or speed won't change. Accordingly, the pressing factor distinction correlates with the liquid stream rate utilizing Bernoulli's condition. The absolute power at every mark of the liquid is steady; the complete power comprises of pressing factor power, dynamic power, and expected power



**Figure 1: Cross sectional sight of venturi**

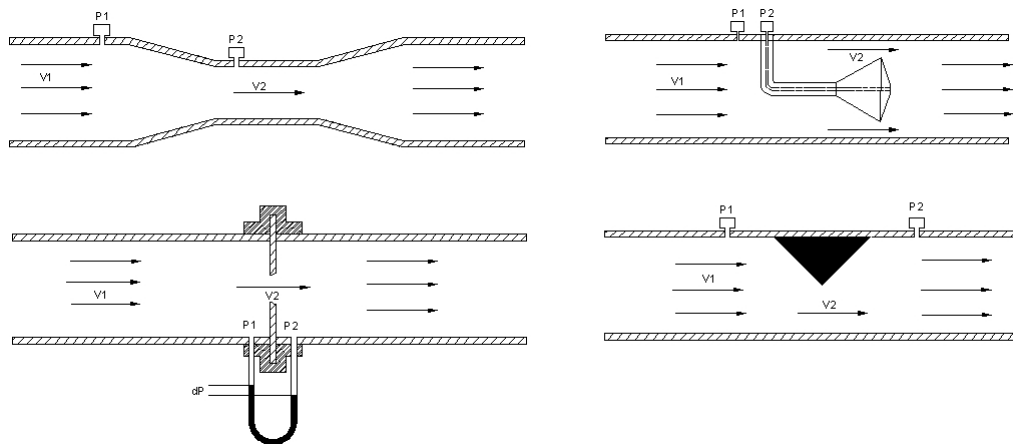
Because of there being an expanded requirement for precise stream estimations of gooey liquids through different sorts of differential pressing factor stream gauges, PC reproductions were led as a feature of this examination to all the more precisely characterize the attributes of the release coadjuvant, (C) at little Reynolds information. The weighty lubricate business has discovered that with growing lubricate costs it has gotten extra affordable for organizations to seek after the withdrawal of amazingly gooey oils, which brings about little Reynolds statistics moving during the line plus thus the gauge . Exact stream estimation is probably the best worry among numerous businesses, since vulnerabilities in item streams can cost organizations extensive benefits. As of now there is mostly secret concerning the C qualities at little Reynolds (Re) information for the gauge in this account since adjustments for these gauges are by and large acted in a lab utilizing chilly irrigate. Differential pressing factor gauges are mainstream for these applications since they are moderately modest plus create dependable outcomes.

Four distinct kinds of discrepancy pressing factor stream gauge were contemplated which comprise: Venturi, normal concentric opening cover V-cone, plus lodge stream gauge. The Venturi stream gauge gets a pressing factor differential by choking the stream region and hence expanding the speed at the tightening, which makes a inferior force as per Bernoulli's Theorem. The concentric hole coat stream gauge diminishes the pressing factor by driving the liquid during



a slender plated round aperture more modest than the line measurement. The V-cone stream gauge has a funnel molded deterrent in the center the line, which powers the stream about the external of the funnel making a 2 pressing factor discrepancy. The block stream gauge has a block molded hindrance situated in the higher part of the line, which diminishes tension on the downstream surface of the block.

The consistency of a liquid is contrarily relative to the Reynolds integer for a particular stream, so expanding the thickness of the liquid outcomes in a more modest Reynolds numeral for a gooey liquid. With an expanded precision in mathematical demonstrating throughout the long term, it is presently conceivable to utilize it for stream conditions where test systems might be deficient. Thick liquids with little Reynolds numbers can't precisely be tried in the research center with water on the grounds that the pressing factor contrasts are excessively little to precisely gauge. Accordingly, PC demonstrating reenactments can be utilized to portray the release coadjuvants over little Reynolds statistics. The entirety of the PC replica reenactments were confirmed by contrasting them with lab information or past discoveries where the release coadjuvants were notable. When the mathematical replicas were checked they were taken to more thick areas where test information with irrigate would have a serious level of vulnerability.



**Figure 2: Sketches of examined pour gauges**

Reynolds information merit unnecessary perception with regards to examining the capacities of stream gauges. The worth of  $Re$  for a specific line stream can be diminished by either diminishing speed, or expanding the liquids thickness. As the thickness of a liquid expansions ready to go, the subsequent divider shear rate diminishes bringing about a more uniform stream

profile . Thusly, to get exact CFD information for minuscule it was important to build the thickness of the streaming liquid which for this examination was a reasonable substantial oil rough consistency of two hundred centipoise

## 1.1 Venturimeter

Venturigauge is a gadget that is exploited to count the pace of stream of fluid during a line. This gadget depends on the rule of Bernoulli's Equation. Venturigauge is named after G.B Venturi who fostered the standard of venturigauge in 1797 yet this guideline comes into consideration with the support of C. Herschel who fostered the first venturigauge in 1887.

Primary pieces of venturigauge :-

1. **Covering part** : It is the piece of the venturigauge where the liquid unites .
2. **Throat** : It is the bit that lies in the middle of the combining and separating part of venturi. In the throat parcel the cross segment is substantially less than meeting and veering segment. At the point when the arrives at the throat, its speed increments and pressing factor diminishes.
3. **Wandering part** : It is the piece of the venturigauge where the liquid gets veers and the cross-segment region increments.

As expressed above it has three sections uniting part, throat and veering part. These three sections are masterminded in efficient request.

Initial one is gulf area or meeting segment. It is the district where the cross area arises into tapered shape for the network with the throat locale. . In this part cross segment region diminishes from starting to finishing. This part is associated with delta pipe toward one side and tube shaped throat on the opposite end. The point of combination is for the most part 20-22 degrees .

Second one is round and hollow throat .It is the center piece of the venturigaugue. It is the tube shaped line in venturigaugue through which the liquid passes subsequent to combining in the united area. Throat has commonly a width of throat is a large portion of the measurement of line. The breadth of the throat stays same all through its length.

Last one is veering segment . It is the finish of the venturigaugue. On one side it is connected to throat of venturigaugue and on the opposite side it is joined to the line. The different segment has a point 5 to 15 degrees . The wandering point is not exactly the uniting point on the grounds that the length of the separating cone is bigger than joining cone. The fundamental explanation of the little wandering point is to stay away from stream seperation from the dividers.

Venturigaugue works on the norm of Bernoulli's condition i.e when speed grows pressure reduces . Cross section of throat isn't actually cross piece of channel pipe. Since the cross - fragment lessens from cove line to throat, the speed of the fluid additions and thusly the squeezing factor reduces. In light of decrease in pressure, a squeezing factor contrast is made between the inlet line and throat of the venturigaugue . This squeezing factor qualification can be assessed by setting a differential manogauge between the channel portion and throat region or by using two guages under control fragment and throat. Ensuing to getting the squeezing factor contrast stream rate through pipe is resolved.

Consider a venturigaugue is fitted in an even line through which fluid ( water ) is spilling as shown in figure under.

Let  $a_1$  = cross-segment space of channel pipe

$d_1$  = width of channel pipe

$v_1$  = speed at channel pipe

$p_1$  = pressure at channel pipe

moreover,

$a_2$  = cross-segment space of throat

$d_2$  = width of throat

$v_2$  = speed at throat

$p_2$  = pressure at delta throat

Applying Bernoulli's equation at segment one and two, we get

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{v_2^2}{2g} + z_2$$

As the pipe is straight, so  $Z_1 = Z_2$

Hence we get,

$$\frac{p_1}{\rho g} + \frac{v_1^2}{2g} = \frac{p_2}{\rho g} + \frac{v_2^2}{2g}$$

$$\frac{p_1 - p_2}{\rho g} = \frac{v_2^2 - v_1^2}{2g} \quad \dots \dots \dots (1)$$

$(P_1 - P_2) / \rho g$  is the dissimilarity of force skull at segment one and two and is equivalent to  $h$ . So eq one become

$$h = \frac{v_2^2 - v_1^2}{2g} \dots \dots \dots (2)$$

Now relating permanence at segment one and two, we get

$$a_1 v_1 = a_2 v_2$$

$$v_1 = \frac{a_2 v_2}{a_1}$$

Insertion the worth of v1 in eq two and resolving, we get

$$v_2 = \frac{a_1}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$$

Now , speed of pour of liquid or release q can be affirmed as

$$Q = a_2 v_2$$

Alternate worth of v2 in this equation, we get

$$Q = \frac{a_1 a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$$

Q is the the hypothetical release beneath perfect circumstances. Real free will be fewer than this.

The real release is given by,

$$Q_{act} = C_d \frac{a_1 a_2}{\sqrt{a_1^2 - a_2^2}} \sqrt{2gh}$$

Where  $C_d$  is coadjutant of venturigauge and its worth is forever fewer than one.

## 1.2 CFD Techniques

Computational liquid elements demonstrating depends on the standards of liquid mechanics, using mathematical techniques and calculations to tackle issues that include liquid streams.

Replicas can incorporate substance responses—ignition measures—with liquid streams to give a

three-dimensional comprehension of heater execution. CFD replicas endeavor to reenact the connection of fluids and gases where the surfaces are characterized by limit conditions. They additionally track the progression of solids through a framework. These replicas utilize the standards of the Navier-Stokes conditions. Reproductions are then led by tackling the conditions iteratively as either a consistent state or transient condition.

Since cold stream demonstrating and CFD displaying now overwhelm the field, and on the grounds that they have critical explicit applications to fuel mixing and the conduct of fuel mixes, they are inspected in more detail in ensuing areas of this part. Actual displaying and CFD demonstrating give a premise to a large number of the mix choices.

CFD displaying gives important data as far as security in the scattering of harmful gas in complex conditions, either in outside climate, for example, in metropolitan regions with different hindrances and building structures, or indoor climate with complex stream bearing. There are various difficulties related with this sort of displaying, like the necessity of exact show of complex calculations, the kind of harmful materials, the delivery sources, the ecological variables, the communication between poisonous materials stream and hindrances, the potential responses with climatic gases or dampness, the chance of buildup, the scattering in outrageous climate conditions or under the impacts of different sorts of occurrences.

### **1.3 Analysis of CFD Replicating**

CFD is the abbreviation for 'computational liquid elements' and, as the name recommends, is the part of liquid mechanics that utilizes PCs to dissect the conduct of liquids and actual frameworks. CFD displaying and examination turned into a mainstream online recreation arrangement as the trouble filled in applying the laws of physical science straightforwardly to genuine situations to make scientific forecasts. This reality turned out to be particularly pervasive for liquid stream and warmth move designing issues.

This is the place where mathematical examination and PCs come in to play; online reproduction. By utilizing mathematical approximations, CFD transforms the full differential conditions into frameworks of direct conditions, which are then settled to acquire field esteems like speeds,

pressing factors, and temperatures on a limited (however frequently huge) number of focuses in the area of the issue.

Albeit mathematical techniques for acquiring inexact answers for differential conditions have existed for a long time, the capacity of PCs to store a lot of mathematical information and perform quick procedure on them is the thing that has transformed innovation into the most functional device for physicists and designers. Simultaneously, this implies that one regularly tracks down that the utilization of CFD to viable issues is restricted by the computational force accessible.

CFD examination considers the demonstrating of liquid due to its flexibility in mathematically addressing conditions of state and actual conduct, communicated in differential or express structure. Additionally, CFD displaying investigations as warmth move issues are of central reasonable pertinence, any equipped recreation device incorporates modules to ascertain temperature dispersions close by pressing factor and speeds. Likewise, a few applications can likewise incorporate examination of solids for versatile disfigurement or compound responses, among other non-liquid applications.

- Move through funneling and adornments like valves, tees, and decreases, to foresee pressure drops, speeds, and vortex developments.
- Vehicle streamlined features, including auto and airplane, to anticipate drag, lift, and downforce.
- Wind designing for structures and wind examination, to anticipate wind powers, vortex arrangement, and person on foot solace.
- Air conditioning frameworks, to survey the presentation of channels or improve warm solace for fake or regular ventilation and for energy utilization.
- Warmth exchangers, to foresee heat move and pressing factor drops.
- Hardware cooling, to anticipate normal and constrained cooling systems execution.
- Windmills, to anticipate cutting edge lift, speed, and force age at given breeze speeds.

- Contamination scattering and airborne pollution control, cleanroom plan.
- Boat and seaward designs for hydrodynamic execution.

## **1.4 Problems of CFD Replicating**

The issue is characterized over a shut math, alluded to as the 'space' encased by its 'limit'.

The marvels to be reenacted is clear cut, like the presence of warmth move, fierce stream, compound responses, numerous stages, various bodies, and so forth, with known material properties and coadjuvants for state conditions.

Beginning qualities, just as qualities on the limits for the thought about fields, are known. This may incorporate pressing factors, stream speeds, dividers, temperatures, heat sources, and so forth

The calculation of the area is parted into little fundamental shapes known as 'cells'. The arrangement of all cells is known as the 'network'. The size of cells will decide the accuracy of the arrangement (the more modest the better), however the number utilized will characterize the interest for PC memory (the more modest cells, the higher tally, the more memory will be devoured, the more extended time the arrangement interaction will take).

## **1.5 Ansys Fluent**

Ansys, Inc. is an American association arranged in Canonsburg, Pennsylvania. It makes and publicizes multiphysics planning entertainment programming for thing setup, testing and movement and offers its things and organizations to customers all throughout the planet. Ansys was set up in 1970 by John Swanson. Swanson offered his benefit in the



association to financial backers in 1993. Ansys opened up to the world on NASDAQ in 1996. During the 2000s, Ansys acquired different other planning plan associations, getting additional development for fluid components, contraptions plan, and distinctive actual science examination. Ansys transformed into a section of the NASDAQ100 record on December 23, 2019. The idea for Ansys was first achieved by John Swanson while working at the Westinghouse Astronuclear Laboratory during the 1960s. By then, engineers performed restricted part examination (FEA) by hand. Westinghouse excused Swanson's arrangement to robotize FEA by making all around helpful planning programming, so Swanson left the association in 1969 to cultivate the item in isolation. He set up Ansys under the name Swanson Analysis Systems Inc. (SASI) the next year, working out of his farmhouse in Pittsburgh

Swanson cultivated the hidden Ansys programming on punchcards and used an incorporated worker PC that was rented continually. Westinghouse utilized Swanson as a counselor, under the condition that any code he made for Westinghouse could in like manner be associated with the Ansys item offering. Westinghouse similarly transformed into the essential Ansys customer.

## **1.6 Features of Ansys Fluent**

### **1.6.1 Meshes, Numerics and Parallel Processing**

Ansys Fluent programming utilizes formless lattice innovation. The cross section can comprise of components in shapes like quadrilaterals and triangles for 2-D reenactments and hexahedra, tetrahedra, polyhedra, crystals and pyramids for 3D recreations. Complex numerics guarantee exact outcomes on some blend of cross section types, incorporating networks with execution hubs and non-coordinating with network boundary. Ansys Fluent's solvers sprint vigorously plus effectively for every actual model and stream kind, consistent condition or fleeting and incompressible throughout hypersonic. Progressed equal preparing capacities, accessible on Windows, Linux, and UNIX stages can be utilized to run reproductions on multi-center processors with different processors on a solitary mechanism and various equipment on an organization. Utilizing 64-cycle innovation, Ansys Fluent can run equal estimations on networks comprising of a billion cubicle or supplementary. Progressed active burden adjusting naturally

rearranges estimations between processors to acquire the most productivity. Regardless of the number of processors are utilized for equal computation, 2 to at least 1024, Ansys Fluent guarantees that CFD estimations profit with the extra preparing power.

### **1.6.2 Dynamic & Moving Mesh**

The unique lattice ability in Ansys Fluent addresses the issues of testing claim, remembering for chamber streams, valves and store partition. A few diverse lattice modifying plans, counting layering, even and remeshing, can be utilized for various touching fraction inside a similar reenactment depending on the situation. Just the underlying cross section and a depiction of the limit development are required. An inherent six-levels of-opportunity solver is additionally accessible for function with unrestrained movement, with amass division, transport hydrodynamics, rocket dispatch, and boiler sloshing. Dynamic cross section is viable with a large group of different models including Ansys Fluent's set-up of splash separation and burning replica and multiphase replica counting those with the expectation of complimentary surface forecast and compressible stream.

Ansys Fluent likewise gives sliding lattice and numerous reference outline models that have a demonstrated history for blending tanks, siphons, and turbomachinery.

### **1.6.3 Turbulence & Acoustics**

Ansys Fluent offers an unrivaled expansiveness of choppiness models, for example, a few adaptations of the revered k-epsilon replica, the k-omega replica and the Reynolds pressure replica (RSM). Ongoing progressions in disturbance displaying have guide to the execution of extra replica like violent change replica, significant for point by point demonstrating of the progress from laminar to fierce stream that happens close to limits, and a Scale Adaptive Simulation (SAS) choppiness model (beta usefulness) which gives a consistent arrangement in stable stream locales while settling choppiness in fleeting hazards like huge partition zones, without an express framework or timestep reliance. Ongoing expansions in PC power, combined with diminishes in processing price, have made the enormous whirlpool reenactment (LES) replica and the additional efficient confined swirl recreation (DES) model appealing decisions for mechanical reproductions. For acoustics, ANSYS FLUENT can register the commotion coming about because of precarious pressing factor variances severally. Fleeting LES forecasts

for exterior pressing factor can be changed over to a recurrence range utilizing the inherent Fast Fourier Transform (FFT) apparatus. The Ffowcs-Williams and Hawkings acoustics relationship can be utilized to display the engendering of acoustics hotspots for different items, going from presented feign bodies to turning fan sharp edges. Broadband commotion source models permit acoustic sources to be assessed dependent on the consequences of consistent state reenactments.

#### **1.6.4 Heat Transfer, Phase Change & Radiation**

Warmth move goes with numerous liquid stream wonders and Ansys Fluent present a complete set-up of alternatives for convection, transmission and emission. A few emission replica are accessible, counting the P1 and Rosseland replica for optically chunky, taking an interest medium, and the examination reason support plane to plane replica for non-partaking medium. The separate ordinates (DO) replica is additionally accessible and appropriate for any intermediate, counting beaker. Furthermore, a sunlight based burden model is accessible for environment manage reproductions and double warmth exchanger replica are accessible.

Different capacities firmly connected with heat move incorporate replica for cavitation, compressible fluids, covering transmission, genuine chat and soaking vapor.

#### **1.6.5 Reacting Flow**

Substance response demonstrating, particularly in tempestuous circumstances, has been a sign of Ansys Fluent programming since its initiation. Ansys Fluent utilizations more up to date models, for example, the swirl scattering idea, PDF transport and solid limited rate science models, just as full grown models like the whirlpool dissemination, harmony blend portion, flamelet and premixed burning replica. In-situ versatile organization (ISAT) can be utilized related to also the EDC or PDF bring replica and gives speed increase to tempestuous limited rate science, accelerating computations by a significant degree or added The normal responding stream replica

accessible in Ansys Fluent can be utilized to handle a huge range of vaporous, coal and fluid fuel burning reproductions. Exceptional replica for the forecast of SO<sub>x</sub> development and NO<sub>x</sub> arrangement and annihilation are additionally accessible. Ansys Fluent's outside response capacity takes into consideration responses among gas and surface species, just as between various species, with the goal that affidavit and drawing can be thoroughly anticipated. Ansys Fluent's response models can likewise be utilized related to the genuine gas model and LES and DES disturbance models.

### **1.6.5 Multiphase**

Ansys Fluent is an innovator in multiphase displaying innovation. Its differed capacities permit designers to acquire understanding into hardware that is regularly hard to test. Ansys Fluent utilizes the Eulerian multiphase replica with its different arrangements of liquid conditions for interpenetrating liquids or stages, just as offering a more conservative combination model. The two models can likewise deal with granular streams. A few other multiphase models are additionally normal in Ansys Fluent. For some multiphase request, for example, splash dryers, fluid fuel showers, constant fiber picture and petroleum heaters the separate stage replica (DPM) can be utilized. The degree of liquid replica is accessible with the expectation of complimentary surface streams, for example, sea waves, where the forecast of the border is of interest. The cavitation replica has demonstrated helpful for powerfully displaying hydrofoils, siphons and fuel injectors. A few populace equilibrium replica are likewise accessible for demonstrating size disseminations.

### **1.6.6 Post-Processing and Data Export**

Ansys Fluent's post-handling apparatuses can be utilized to produce significant designs, movements and reports that make it simple to pass on CFD results. Concealed and straightforward surfaces, pathlines, vector plots, form plots, custom field variable definition and scene development are only a portion of the post-preparing highlights that are accessible. Arrangement information can be sent out to Ansys CFD-Post, outsider illustrations bundles, or to CAE bundles for extra investigation. Under the Ansys Workbench climate, Ansys Fluent arrangement information can be planned to Ansys reenactment outside for employ as warm or

pressing factor many. In independent form, Ansys Fluent, can likewise plan primary and warm many on exterior and hotness in amount from Ansys Fluent to outsider FEA networks.

### 1.6.7 Customized Tools

Client characterized capacities are a well known alternative for clients needing to modify Ansys Fluent. Thorough documentation and various instructional exercises are accessible, as is full specialized help. The Ansys worldwide counseling organization can give or help make formats to the rehashed arrangement of any hardware. Extra modules for some, uncommon applications are accessible, for example, PEM and strong oxide power devices and manage to hydrodynamics.

### 1.7 Math and cross section

Venturi configuration is a cycle with emphases to formalize last math replica. In this examination, the cycle is finished with the united and different points of venturi to get anticipated plan. Math for three diverse focalized and unique points was done in CREO 3.0. With estimating the areas, characterized calculation boundaries are demonstrated in CREO 3.0 including joined points ( $\theta$ ), unique points ( $\emptyset$ ) and gullet measurement ( $d$ ). The line breadths for a given venturi replica kept 40 millimeter for together gulf plus passage area. The gullet divide is twenty four millimeter in given replicas for venturi plan. The absolute span of venturi counting merged and unique is one hundred thirty five millimeter.

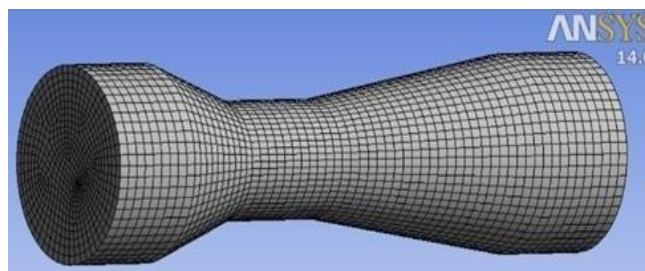


Figure 3: Meshed replicating of venturi geometry type one

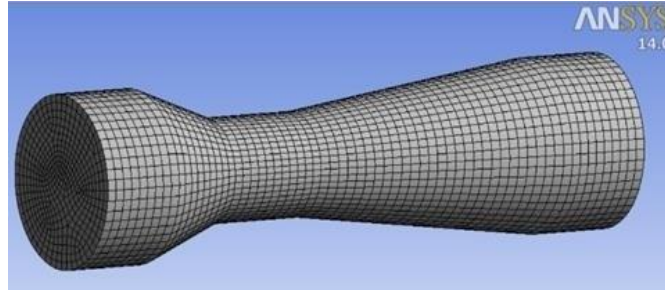


Figure 4: Meshed replicating of venturi geometry type two

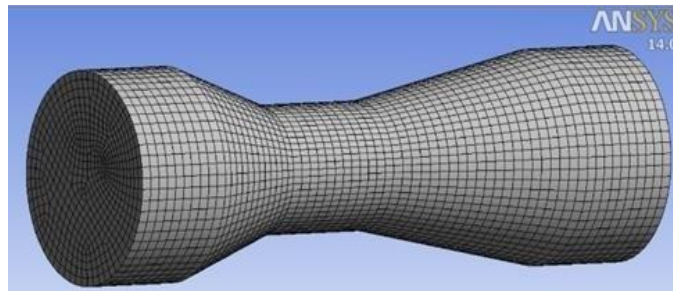


Figure 5: Meshed replicating of venturi geometry type three

## 1.8 Objectives

The essential destinations of this proposition were as per the following:

- 1) Evaluate the chance of a mathematical PC arrangement by utilizing ANSYS FLUENT
- 2) Perform a broad measure of reproduction on the various replicas being investigated.
- 3) Provide rules for the utilization of these stream gauges at little Re numbers.
- 4) Provide a broad scope of release coadjuvants qualities for these four kinds of differential creating stream gauges.

The hypothetical foundation of FLUENT© and stream gauge conditions will then, at that point be introduced. This will be trailed by the cycle utilized for setting up the reenactments and a technique to empower the expectation of the release coadjuvants for the stream gauges. The genuine mathematical methodology will then, at that point be completely depicted alongside the

comparing replica outcomes. At last the discoveries from the outcomes will be summed up and introduced to exhibit their helpful uses to the stream gauge commerce

## CHAPTER 2 : REVIEW OF LITERATURE

**Cassidy (1965)** utilized mathematical technique to investigate spillways and get power scattering. In this investigation, Cassidy endeavored to decide tension on the peak of an Ogee spillway in 2 dimensional space

**Sorensen (1985)** thought about power dispersal rate in Ogee and ventured spillways. Likewise, power dissemination speed in ventured spillways was accounted for about seventy five percent additional than Ogee spillways. Likewise, stilling bowl measurements demonstrate an overall diminishing of eighty four percent

**Pegram et al. (1999)** directed an exhaustive report to research the impact of mathematical attributes of steps and scale on the sort of stream and power dissemination speed, with the presumption of making equilibrium circumstances at the downstream of the stream. In this exploration, estimating stream power in downstream of the ventured and Ogee spillway, which was dimensionally comparable, power dissemination speed in ventured spillway was accounted for higher. Besides, the got consequences demonstrate that power dissemination is diminished by the expansion of spillway incline

**Tabbara et al. (2005)** utilized limited component technique to register water stream outline over ventured spillway utilizing ADINA-f programming. They likewise utilized normal replica of  $K-\epsilon$  to decide stream disturbance. The figured irrigate stream profile with respect to all developed ventured spillways was subjectively in understanding to stream qualities and quantitatively like the deliberate upsides of gratis exterior stream outline. Also, relation power dispersal was figured and contrasted with the qualities acquired by the test. As uncovered, there was a decent agreement between the mathematical and exploratory qualities

**Mansoori and Pedram (2008)** contemplated end ledges ventured spillway and introduced a connection to decide power scattering pace of these spillways. They utilized twenty three stages completed of plexi goblet (with the width of ten mm, the span of seventeen cm, the breadth of fifty five cm, and the height of 3 cm) from the top associated with a metal skeleton and plexiglass dividers. They played out their trials with releases of 3.6 lit/s (Nappe stream) and 25



/ (Skimming stream) and took standing pressing factor forced on floor and its vacillations with stream speed and profundity. Investigating the acquired information and changing Rajarantnam and Chamani's condition, they could introduce a connection to decide energy dissemination rate in end ledge ventured spillway at Nappe stream system. They at last reasoned that the presence of ledge would impacts energy dissemination rate in ventured spillways; nonetheless, this impact on stream has an alternate pattern and diminished by the expansion of release. In Nappe Flow system, width, stature and heavenly messenger of ledge at upstream would impact energy dispersal rate; all in all, expanding width and tallness of ledges increment power dissemination rate and diminishing the heavenly messenger of ledge at upstream would diminish energy scattering. Along these lines, vertical ledge contrasted with bend ledge causes superior power dissemination however in Skimming stream system, the impact of ledges on power dispersal is slight because of ledges' misfortune

**Naderi Rad et al. (2009)** researched energy dispersal in different kinds of ventured spillways counting straightforward, ledges, and slanted ones utilizing FLUENT mathematical replica. Absolutely, 33 mathematical models were made counting eleven ventured spillway gatherings. These eleven gatherings were examined for three releases and three limit conditions. To investigate basic ventured spillways, five model gatherings were measured for every one of them, three releases (0.0190, 0.537 and 0.0987 m<sup>3</sup>/s, spillway plan tallness (hd) of 0.05, 0.1 and 0.15 m and basic stature (Yc) of 0.0334, 0.0667 and 0.1 m were dissected. For every one of the ledges and inclined ventured spillways, three model gatherings were thought of. Each gathering was examined for three releases (0.0190, 0.0537 and 0.0987 m<sup>3</sup>/s, spillway plan stature (Hd) of 0.05, 0.1 and 0.15 m and basic tallness (Yc) of 0.0334, 0.0667 and 0.1 m were broke down. Expanding the quantity of steps when the tallness of dam is consistent, causes the increment of energy scattering in ventured spillways. Diminishing ventured spillways' slant when the stature of dam is steady causes the increment of energy dissemination. expanding the slant of steps' floor when the dam stature, number and size of steps just as the spillway incline are steady, causes the increment of energy scattering in the slopped ventured spillways. Expanding release in every one of the three conditions of the ventured spillways grounds the diminishing of power dispersal and power scattering transform is a sort of free stream

**Mansoori and Soori (2013)** thought about energy dissemination in Nappe stream system and Skimming stream system utilizing FLOW-3D. As well as examining the determination of stream type in ventured spillways, they broke down recently detailed outcomes. Then again, they researched trial connection introduced to process energy scattering. The investigation depended on the equation introduced by Stephenson . To such an extent that, they thought about the general power scattering got by FLOW-3D with the worth acquired by Stephenson's condition. The outcome acquired by the mathematical model and Stephenson's connection was predictable.

**Hamedi et al. (2016)** investigated four stages (39 to 42) of a 60-venture spillway and examined that by the utilization of FLUENT. The four stages with slant and ledge were put at the same time. Different ledge with various tallness and thicknesses were tried. In three stages, invert slants of 7, 10 and 12 were applied. Dimensionless boundary  $h$  was utilized to gauge energy scattering. The got results uncovered that in the release of 30 / (release per unit width = 0.0225 2/ ), which demonstrates Nappe stream system, the means with synchronous slant and ledge (where the proportion of m/h is under 0.7) altogether builds energy dissemination

**Diminished Order Modeling (ROM):** ROM is a strategy for superseding the principal model with much more unassuming solicitation model that can regardless depict critical wonder of an association with worthy precision. The major idea behind ROM is to find a lessened reason which has thorough and through diminished number of levels of chance diverged from the main course of action of the model. The most notable way to deal with track down an optimal reason is by Proper Orthogonal Decomposition (POD). Case is an authentic model assessment to find the prevalent plan. For detail of ROM and POD we imply. Multiplication for fluid stream, heat move were done in and independently. Brenner, T. A., et. al has handled multiphase warmth transfer issue using ROM where they found magnificent simultaneousness with the full solicitation model, in their paper they have discussed diverse practical issues of POD. Lappo, V. also, Habashi, W, and Lieu, T., et. al. has achieved constant amusement using ROM, where Lieu, T., et. al. has exhibited a full plane course of action and the results were promising.

**Marker and Cell (MAC) procedure:** MAC is a system subject to restricted difference staggered structure introduced by Harlow and Welch. It was at first planned to settle free surface streams. They used marker particle to stamp the cell containing fluids and track the improvement of the surface by presentation. For nuances of the main MAC we imply. An enhanced type of MAC called SM

AC with the assumption for free surface stream generally space was portrayed in. A joined method using FEM and MAC was made to settle Navier-Stokes condition. A structure heat move issue was gotten comfortable. For the most part incredible composing review was done by McKee, S., et. al. Furthermore, they have assessed the new upgrades in MAC in

**Smoothed Particle Hydrodynamics (SPH):** SPH strategy is a molecule based technique created by Gingold and Monaghan (1977) and Lucy (1977) initially to take care of astronomy issues however it got quite possibly the most grounded strategies in CFD. In SPH plan, liquids are addressed by separate element and the belongings of the element are then round by bit capacities over the element inside a specific span. A wide scope of liquid stream and warmth move issues were tackled by this strategy to accomplish constant or close to continuous reproduction with a respectable exactness. An excellent outline on the new improvements on SPH technique has been summed up in by M. B. Liu and G. R. Liu. SPH is very grounded to tackle multiphase and free surface issue as of late. An examination on utilization of SPH to multiphase stream was finished by Szewc, K. et. al. in. Complex free surface and multiphase issues were addressed in and, where they demonstrate talented implementation of SPH to catch boundary. Warmth move issues were addressed in, and with an excellent precision. SPH executions were done in and to tackle different CFD issues progressively.

**Quick Multipole Method (FMM):** FMM is a molecule strategy created by L. Greengard and V. Rokhlin in 1997. Later on in 1999 by Cheng, H., et. al. a versatile adaptation of FMM was introduced to settle Laplace conditions in 3D. FMM ascertains the power between particles utilizing the multipole development. The more term we have in the development, the more exact the model is. One can handle the precision and speed utilizing this strategy. Greengard and Kropinski utilized FMM to compute the volume fundamental of incompressible Navier-Stokes conditions and accomplished execution  $\square$   $\square$  or  $\square$   $\square$ , where  $\square$  is the quantity of focuses in the discretization of the area. As of late, a petascale choppiness close to continuous reproduction was finished by Yokota, R., et. al., in utilizing GPU engineering.

**Technique for Fundamental Solutions (MFS):** MFS is a method of taking care of certain elliptic limit esteem issue previously proposed by Kupradze and Aleksidze in 1964. In MFS the surmised arrangement is communicated as a direct mix of principal arrangements. The fundamentals and the subtleties of this technique can be found in the book. Incompressible

Navier-Stokes conditions were tackled in and interface issues in. Warmth move coefficient was assessed for complex issues in and utilizing MFS.

**Limited Pointset Method (FPM):** FPM is a molecule technique for continuum mechanics issues like liquid stream. It has been all around adjusted to mimic different complex time subordinate streams, moving surface, free surface and warmth move issues. FPM has beaten the principle downside of lattice based strategies which is the re-cross section for time subordinate moving surface streams. The Fraunhofer bunch in Germany has fostered a model on FPM to reenact many fascinating issues like refueling the engine vehicle, airbag sending and so forth Incompressible Navier-Stokes conditions were tackled in and multiphase issues. Utilization of FPM to the warmth conduction issues are talked about in.

**Moving Particle Semi-Implicit Method (MPS):** MPS is additionally a molecule technique uniquely intended for reproducing incompressible free surface stream created by Koshizuka and Oka in 1996. MPS is like the SPH technique, nonetheless, MPS applies easier differential administrator as opposed to taking angle of portion work like SPH. Tokura did an examination among SPH and MPS utilizing LS-DYNA (programming bundle) and found that MPS plays out somewhat preferable for certain issues over SPH because of its straightforwardness. There are numerous accessible articles on free surface streams utilizing MPS, and especially are with regards to our advantage.

**Quick Fluid Dynamics (FFD):** FFD is a middle methodology between network free and cross section based technique for settling Navier-Stokes conditions. It was first presented by Zuo W. also, Chen Q. in to mimic ongoing or quicker than continuous reenactment of wind current in structures. As indicated by the creators, the FFD technique was educational yet less precise than CFD. They have executed their strategy in GPU and accomplished 500-1500 times quicker reenactment than CFD on CPU. Jin, M., et. al., in has mimicked lightness driven streams inside structures in extremely huge scope. A few improvement were likewise done subsequently to build the precision of FFD strategy.

**Molecule in Cell Method (PIC):** PIC is a crossover approach where particles are utilized to address the properties of the liquids. The information is then moved to a matrix from particles to insert the qualities between particles. It was very effective strategy in plasma reenactments in mid 1960s. Besides, this technique was likewise used to tackle complex CFD issues for instance high-energy atomic crash in and stun and rarefaction streams in multiphase combination . Progressed issue like fluidized bed was addressed utilizing PIC.

**Vortex in Cell Method (VIC):** Vortex technique is a class of strategies that settle the vorticity condition rather than force condition. The issue with vorticity condition is that it doesn't give the speed straightforwardly. To get the speed field, it is needed to settle the Biot-Savart law, which requires a huge PC time. Notwithstanding, VIC strategy can beat this disadvantage by utilizing a semi-Lagrangian approach. VIC moves the vorticity particles to a network and addresses the Poisson condition to get the speed field. VIC was utilized to show incompressible streams in 3D, disturbance in 2D and vortex structure in 3D.

**Cross section Boltzmann Method (LBM):** LBM is an alternate class of CFD techniques which address the Lattice Boltzmann condition rather than Navier Stokes conditions. It shows liquid stream by utilizing a molecule network approach where the particles dwell at the hubs of a discrete cross section network. For a prologue to LBM and its application in designing . An awesome outline on LBM for single and multiphase streams just as the new improvement on LBM . Expansion to LBM, a Thermal LBM for multiphase stream and warmth move . Convective warmth move issue was tended to by Rosdzhimin, A. R. M., et. al in, where they discovered benefits of LBM over straightforwardly tackled Navier Stokes condition as far as Knudsen number. LBM can be utilized to reproduce low Knudsen number warmth move issues. More, complex warmth move issues were tackled utilizing LBM, for example warm conduct of a bead on strong surface , upgraded heat move for nanofluids . Use of LBM empowered scientists to settle complex multiphase and warmth move issue as of late just as accomplished ongoing CFD. For instance, Gevelera M. et. al. in have executed LBM to reproduce different complex liquid stream and accomplished constant reproductions utilizing multi-center engineering.

G.Satish, K.Ashok Kuma, V.Vara Prasad, Sk.M.Pasha concentrated in their paper about the course through abrupt and steady difference in pipe diameter(enlargement and constriction) was mathematically recreated with water by temperamental stream in k-epsilon conspire. The significant perceptions made identified with the pressing factor and speed forms during the time spent move through these lines. Unexpected amplification makes more extreme arrangement of stream swirls than abrupt withdrawal. Additionally, the misfortunes are more at where the expansion in the line starts. In the unexpected constriction, vane contracta's are shaped at the place of compression and impact of consistency is irrelevant on the pressing factor drop through abrupt withdrawal.

Wan Kai,Wang Ping concentrated in their paper about Using standard k-ε model with FLUENT programming on enormous width CFD mathematical reproduction of wind current in a 90 ° bowed cylinder. The standard k-ε model has a place with the whirlpool consistency model, which receives shut RANS conditions to settle the model. The pre-owned liquid medium is the encompassing air, the thickness  $\rho$  to 1.225 kg/m<sup>3</sup>, kinematic consistency  $\mu$  for 1.7894e-5 kg/m.s. Expecting that the wind current pace of 15 m/s the constant and stable way moves through the elbow. As the stream rate is little, it tends to be viewed as incompressible liquid. By homogenization of the coherence condition and immediate Navier-Stokes conditions, the Cartesian facilitate framework under adiabatic, consistent, incompressible liquid stream is administered by the control condition.

**(U.S. Agency of Reclamation, 1987)**The Ogee-peaked spillway is quite possibly the most significant and regular pressure driven designs, its eminent water driven qualities permit it to deliver overabundance water or floods that can't be contained in the capacity volume. Ogee-peaked spillways are regular as water release structures in different circumstances

**(Peltier et al., 2018).**They are proficient and safe when planned and worked with exactness; they additionally measure the stream rates with adequate accuracy. At the point when the pressing factor head arrives at a plan head, a zero relative pressing factor is regularly found along the surface profile

**(Specialists, 1952)** However, an ill-advised plan of this construction can prompt dam-break. Public insights shows that overtopping because of insufficient spillway plan, trash blockage of spillway, or resolution of the barrier peak represent roughly thirty four percent of all dam disappointments in the United States of America; hence, these spillways must be painstakingly intended to confirm stream qualities

**(Savage and Johnson, 2001)** The ogee-peaked spillway is perhaps the most considered pressure driven constructions due to its presentation and its capacity to pass overflow water proficiently and securely with sensibly great stream estimation abilities. Hence, engineers use it's anything but a wide scope of circumstances

**(Kanyabujinja, 2015)** Flow over the Ogee-peaked spillway ought to hold fast to the substance of the silhouette to forestall passage of air under the water sheet. As far as head plan, the stream floats more the exterior shape with insignificant limit shell impedance; this prompts an ideal effectiveness of release.

**Peltier et al. (2015)** There are generally couple of learn on the stream attributes over an Ogee peaked spillway, especially for heads that are bigger than the plan skull. There is additionally no adequate data accessible in regards to the upward speed dissemination along the peak profile approved pressing factor estimations and speed circulations directed in two water powered replica with different scale components of an Ogee spillway. These were worked at skull proportions that are generally more noteworthy than unit

**(Chanel and Thesis, 2009; Ho et al., 2006; Kim and Park, 2005; Savage and Johnson, 2001).** Numerical reenactments are valuable in hydrodynamic examinations counting investigations of stream over Ogee spillways. A correlation of these mathematical outcomes with exploratory information is as yet needed for adjustment and approval. The economically accessible Computational liquid Dynamics programming bundle, Flow-3D, utilizes the limited volume strategy and can tackle issues including liquid stream. The computational area is partitioned utilizing Cartesian directions into a network of changeable measured hexahedral cells. For every cell, the normal qualities for the stream boundaries, for example, pressing factor and

speed are processed at discrete occasions. Most writing on CFD-based displaying of spillways utilizes Flow 3d, which settles the Reynolds-averaged Navier-Stokes (RANS) conditions

PIV is a kind of beat brightness velocimetry (Adrian, 1991; Sveen and Cowen, 2004). It utilizes a particulate tracer to follow liquid relocation. The PIV hypothesis depends on the estimation of little tracer element. These are adequately little to chase the development of the liquid of interest. These subdivision are then enlightened with a meager glow piece. Dispersed light was then put away in ensuing picture outlines with realized stretches utilizing a camera. PIV estimates the whole speed field and figures the removal of the atom inside the given time span by taking two pictures immediately after each a different with fast camera (Fujita et al., 1998). These recorded pictures are then prepared on a PC utilizing Matlab codes to dissect the development of atom in subsections of the PIV pictures through cross relationship strategies. The outcome prompts a molecule picture uprooting design subsequent to thinking about the picture amplification and time delay

**Maynard (1985)** showed four distinct states of the upstream substance of the spillways: one vertical and three slanted. The upstream bend profile is a blend of radii that are comparative with the complete head, while the downstream bend is the bit between the peak pivot and the digression segment.

**(Savage and Johnson, 2001)**The rating bend of the spillway is a significant pressure driven trademark that shows the consistency and exactness of the model. It is determined from hypothetical conditions. The information is recorded with an electromagnetic flowmeter and afterward contrasted and the condition. The flowmeter was settled under the flume to be associated between the radial siphon and the formed bay tank. The hypothetical release through the ogee-peaked spillway can be communicated as portrayed.

**(Falvey, 1990)**. At the point when cavitation happens close to the substantial surface of a spillway, it prompts the plan of fume bubbles. The air pockets are then disintegrated in the water and moved by the stream. Subsequently, the encompassing pressing factor of the air pockets expands, which makes the air pockets not, at this point practical and makes them collapse. The collapses happen at a high recurrence with an amazingly high pressing factor of up to 1,500 MPa.



(Lesleighter, 1988) and incalculably sway the substantial surface. This cycle brings about weariness disappointment of the substantial materials, which then, at that point makes the microcracks in the surface. After some time, these undesired breaks will cause a lengthened opening. As time passes, the opening expands, with the rapid stream affecting its downstream end.

Sheehan (1974) led trial tests on substantial materials and noticed that an air substance of 1–2% considerably diminished the cavitation harms, and with more than 5–7%, no harms were noticed. From model perceptions

Chen et al. (2003) referenced that the cavitation harms were clearly relieved when the air focus nearby the divider was in the scope of 1.5–2.5%. The harms totally vanished if the fixation arrived at 7–8%. An aerator is a savvy gadget that falsely supplies air into the water stream in a spillway. It is put where the cavitation harm may happen. In 1961, the adequacy of air circulation was seen in the Grand Coulee Outlet Works

(Borden et al., 1971). From that point forward, aerators have gotten boundless. An aerator adds to raising the air grouping of the water stream in a chute spillway. At the point when the water moves through the aerator, a free stream is produced, and fierce swirls in the lower fly surface viably entrain air. An air pit is shaped under the stream. During the entraining air by the fly, the pressing factor in the cavity dips under the climatic pressing factor. Accordingly, a pressing factor distinction exists between the cavity and the climate, which permits the air from the air to be sucked into the hole by means of the aerator framework.

Bercovitz et al. (2016) led an enormous scope PIV to investigate the surface speed field of a plunging water fly from a sharp-peaked weir. They intended to consider the nappe direction and trademark length, along which the energy dissemination got noticeable.

**Lin et al. (2008)** applied the BIV and HSPIV techniques to get the speed fields of the air circulation district in a stream at a drop structure. In Papers VII, the creators showed the uses of these estimations and methods to an aerator stream in a flume.

**(Hirt and Nichols, 1981; Hibiki and Ishii, 2000; Kolev, 2005; ANSYS, 2015; Özkan et al., 2016).** These incorporated the Volume-of-Fluid (VOF) Model, Mixture Model, and Two-Fluid Model (TFM). Aerator streams are an air-bubble stream, happening at a high-speed stream speed. It represents a test to mathematical expectations, since the stream speed frequently surpasses 20 m/s and can arrive at 45 m/s in enormous dams. The high speed improves the trade between the air and water, which makes the air transport measure escalated. This infers that plans of the stage connections become confounded in an aerator stream. The fundamental justification this is the absence of model estimation information for mathematical model alignment and check

**(Kökpınar and Göğüş, 2002; Deng et al., 2005; Liu and Yang, 2014; Jothiprakash et al., 2015; Rahimzadeh et al., 2015).** **Aydin and Ozturk (2009) and Zhang et al. (2011)** utilized the Mixture Model to research an aerator stream. They tracked down that the model gave the ideal capacity to reproduce aerator streams, particularly in high air-fixation districts. These examinations focused on both test and model information and showed that the model addressed sensible base pressing factor and air hole profiles.

**(Xu et al., 2001; Zhang, 2008).** The Two-Fluid Model is additionally an elective model for depicting aerator streams. Not at all like the VOF model, it displays the collaborations between air pockets and water, including the stage drag power, the fierce scattering power, and so forth. In related investigations, mathematical outcomes are contrasted and the exploratory information. These examinations show the capability of displaying aerator streams and further rouse assessments and assessments of the TwoFluid Model.

**Aydin et al. (2019)** examined base outlet of Ilisu Dam utilizing CFD model. In the examination, the exhibition of air circulation displays with different plans was researched. Toward the end, two new air circulation plans for that specific circumstance were proposed.

**Chanson (2009)** expressed that the extrapolation of lab results to huge model pressure driven constructions essentially worried in spite of late advances around here and examined the unique likeness of the air entrainment measures. It is noted in the paper that actual model investigations were performed for the most part utilizing Froude similitude rule with more modest Reynolds number than comparing model flow, and the idea of scale effect is firmly related with the determination of significant trademark air–water flow properties.

**Kumcu (2017)** utilized a CFD model with Flow-3D to explore the flow over a full scaled (model) ogee spillway and contrasted with 1/50 scaled actual model outcomes. The aftereffects of the mathematical model well concur with the scaled actual model as far as free-surface qualities like surface level, flow speed and pressure factor, however any information about detail of air entrainment sum and its scale effects were not given other than some air fixation.

**Geun and Hyun (2005)** researched some flow qualities of an ogee spillway by utilizing CFD model (Flow-3D) to notice unpleasantness and scale effects on them. They found that while the surface unpleasantness and scale effects don't affect a few outcomes like release, water surface and peak pressures excessively, the harshness and scale effects are significant in greatest speed area. Ferrari (2010) effectively played out a mathematical report on the freesurface flow over a sharp-peaked weir. The outcomes were approved by contrasting the free-surface profiles got from trial estimations in the writing, and a decent understanding was accomplished.

**Heller (2011)** introduced an audit on the Froude and Reynolds model-model similitudes to portray scale effects for ordinary pressure driven flows and talked about how scale effects were kept away from or adjusted. Felder and Chanson (2017) did some test of high-speed blending flow to explore scale effects concerning air–water flow. They introduced an extensive examination on the air–water flow properties, e.g., the interfacial region, choppiness properties and molecule sizes, which might be affected by scale effects. They likewise expressed that the findings of the examination are relevant to the next air–water flow type, however the model information were required for final confirmation.

It is understanding from above specialists, for scaled model of water powered designs, while the scale effects are insignificant for some flow boundaries, for example, release flow rate, water

surface and pressing factors, it tends to be very significant for high-speed air–water blend flow, e.g., spillway flows with an aerator. In this examination, the spillway aerator of the RRC type dam of 100 m stature was chosen as the model. The mathematical model of the spillway was set up in the model utilizing a computational fluid model in various flow conditions (5223, 3500, 1750 and 1000 m<sup>3</sup>/s of flow rate), and the hydrodynamic conduct of the current plan was examined with the assistance of computational fluid elements (CFD). The got mathematical model outcomes were contrasted and the aftereffects of the model test performed by DSI, and the acquired outcomes were examined introducing the hydrodynamic properties of the current plan (Özcan 2011). The hydrodynamics of the flow on the spillway was first explored with a solitary stage flow model, and a doublephase (air–water) flow model was utilized for aerator execution on the spillway.

**Chadwick et al. (2004)** depicted a spillway as a construction that is a painstakingly planned entry used to accommodate the controlled arrival of water from a dam into a downstream region, ordinarily being the waterway that was being dammed. Spillways discharge floods securely with the goal that the water doesn't up and over the design which could prompt harm or even disappointment of the dam.

**(van Vuuren, et al., 2011)** An abundance of writing is accessible on the guess of the Ogee profile for spillway plan and a few undertakings have been made fostering a relationship that would have the option to numerically depict the state of the Ogee bend thinking about 2-dimensional stream boundaries. Lamentably much of the time the stream over an Ogee spillway can't be thought about only as a 2-dimensional stream state. The asymmetry of valleys and geographical methodology channels where spillways are developed will impact the stream example and speed circulation upstream of the spillway. Disregarding these 3-dimensional stream practices may bring about a deficient plan of the Ogee spillway structure. The most clear 3-dimensional stream boundaries that impact the calculation of the Ogee profile incorporate.

## CHAPTER 3 : MODELING AND ANALYSIS

The test examination has been completed on the arrangement office for venturigaugage plans as talked about in the part of trial methodology. This set up involves two pipelines of forty millimeter and twenty five millimeter width set in equal and preset to the gentle steel (M.S) position. Each line has personality venturigaugage and opening gaugage with force recordings. Both venturi and opening gaugage are fixed in the funneling framework with adequately long line span upstream of the gauges. The pressing factor recordings are associated with a typical center chamber just as the U cylinder disparity manogaugage. The fluid utilized in the manogaugage was mercury (explicit gravity ( $S_w$ ) = 13.6). To manage the course throughout equal pipeline stream manage regulator has been put at the bay and opening of a tube. In this arrangement, the pipeline of forty millimeter distance across was utilized to play out the analyses. As per that, the venturi introduced on a similar pipeline. By opening and shutting the stream control valve which gives the manometric perusing utilizing U cylinder differential manogaugage. The water was gathered in the water assortment tank for the hundered millimter ascent of water level in the comparing tank. The space of compressed water assortment tank was 0.036 m<sup>2</sup>. The stream rate for liquid stream is changed according to systems followed. The liquid stream for the exploratory arrangement controlled through the stream control valve. The perusing esteems were taken at climatic pressing factor of 1 Kpa and temperature of 30 degrees by keeping the particular gravity of water and mercury as a norm. The fall in force head (m) determined by adding the U cylinder differential manogaugage (H1, H2) situated at the concurrent and throat area. To ascertain the coadjuvant of release ( $C_d$ ) worth of hypothetical and genuine stream rate has been learned at the 100 mm ascent of hose plane.

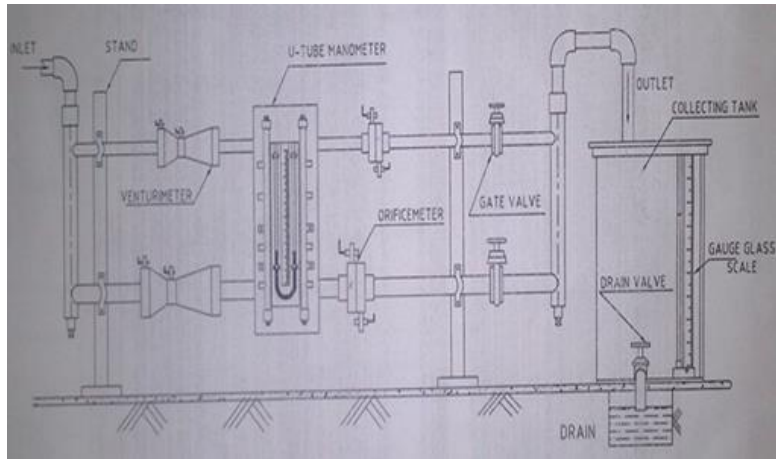


Figure 6: Experimental Replicating setup

TABLE 1: RESULTS OBTAINED WITH EXPERIMENTAL SETUP FOR VENTURIGAUGE								
Geometry type	Venturi Angles ( $^{\circ}$ )		Manogauge Reading (m)		Pressure Drop (m)	Actual Flow rate ( $Q_a$ ) ( $m^3/s$ )	Theoretical flow rate ( $Q_t$ ) ( $m^3/s$ )	Coadjuvant of Discharge ( $C_d$ )
	Convergent ( $\theta_c$ )	Divergent ( $\theta_d$ )	H1	H2	$h = 12.6 (H1 - H2)$	$Q_a = 0.036/t$	$Q_t = 0.002148(h)^{0.5}$	$C_d = Q_a/Q_t$
1	21	9	0.437	0.427	0.1260	$6.79 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.89
			0.435	0.426	0.1134	$7.05 \times 10^{-4}$	$7.23 \times 10^{-4}$	0.97
			0.434	0.425	0.1134	$7.20 \times 10^{-4}$	$7.23 \times 10^{-4}$	0.99
			0.434	0.423	0.1386	$7.20 \times 10^{-4}$	$7.99 \times 10^{-4}$	0.99
2	20	11	0.436	0.426	0.1260	$7.05 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.92
			0.435	0.425	0.1260	$6.92 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.90
			0.434	0.424	0.1260	$7.05 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.92
			0.435	0.426	0.1134	$6.42 \times 10^{-4}$	$7.23 \times 10^{-4}$	0.88
3	21	7	0.434	0.424	0.1260	$7.50 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.98
			0.435	0.426	0.1134	$6.92 \times 10^{-4}$	$7.23 \times 10^{-4}$	0.95
			0.434	0.425	0.1134	$6.42 \times 10^{-4}$	$7.23 \times 10^{-4}$	0.88
			0.430	0.42	0.1260	$6.31 \times 10^{-4}$	$7.62 \times 10^{-4}$	0.82

### 3.1 Type 1

The investigation of venturi areas dependent on computational liquid elements has been led as displayed beneath. The accompanying outcomes for the pressing factor and speed forms are broke down and addressed by the calculation of venturi having joined and disparate points as  $\theta_c = 21$ ,  $\text{Ø}d = 9$

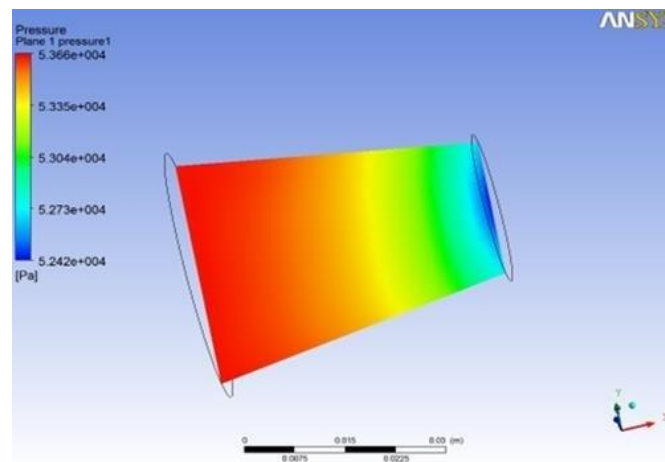


Figure 7: Force difference for venturi replica (ANSYS)

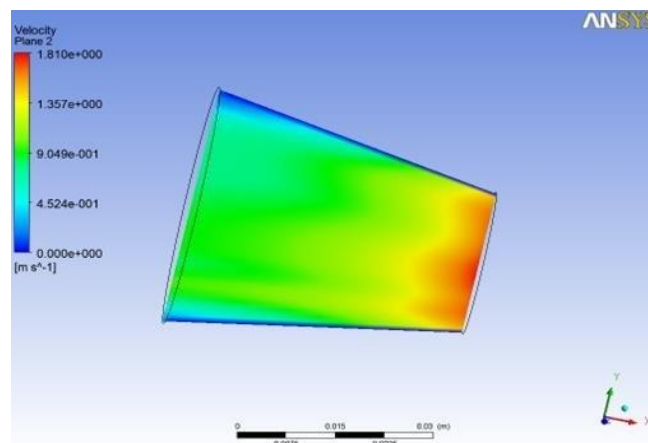


Figure 8: Velocity variation for venturi replica ( $\theta_c = 21$ ,  $\text{Ø}d = 9$ ) (ANSYS)

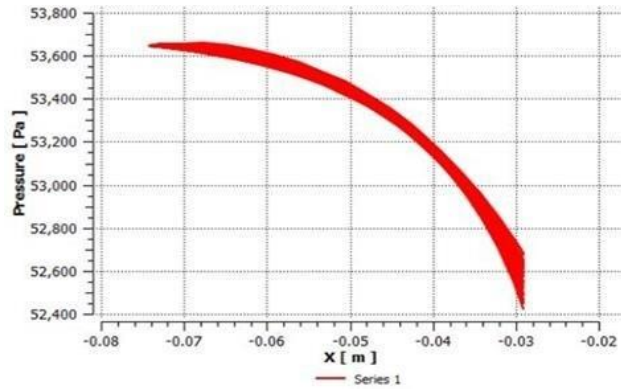


Figure 9: speed difference plot for convergent segment ( $\theta_c = 21$ ,  $\text{Ø}d = 9$ )

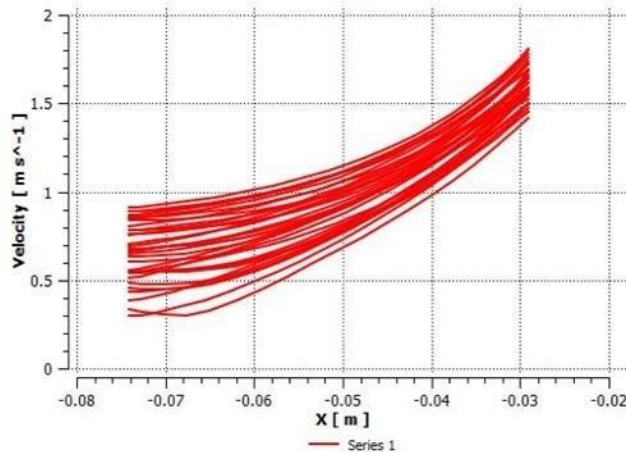


Figure 10: force difference plan for convergent part ( $\theta_c = 21$ ,  $\text{Ø}d = 9$ )

The joined area is assessed for pressing factor and speed variety across X-bearing with pressing factor and speed vector. It reasons that there is a significant fall in force at the united area from 53660.35 Pa to 52420.15 Pa as displayed in figure7 and figure 9. The speed variety from zero to 1.810 m/s (channel to gullet) as displayed in Fig. 8 and Fig. 10 because of progress in the cross-segment at the joined bit. Here 25 emphasess were taken for pressing factor and speed variety



### 3.2 Geometry type 2

For the following arrangement of mathematical replicas having merged point ( $\theta_c$ ) = 20, different point ( $\varnothing d$ ) = eleven has been investigated in CFX solver for computational liquid elements (CFD) calculation. The variety gave in the subsequent math arrangement gives out an extra pressing factor and speed variety athwart X-heading. As the variety in joined and disparate points sway the outcomes planned in figure ten and figure twelve. Variety in force is seen slow, accomplishes esteem from 53770.05 Pa to 52560.25 Pa. figure eleven and figure thirteen shows speed variety for the enture having focalized point ( $\theta_c$ ) = twenty and unique point ( $\varnothing d$ ) = 11. Speed smooth out addresses the variety in speed from 0 to 1.888 m/s.

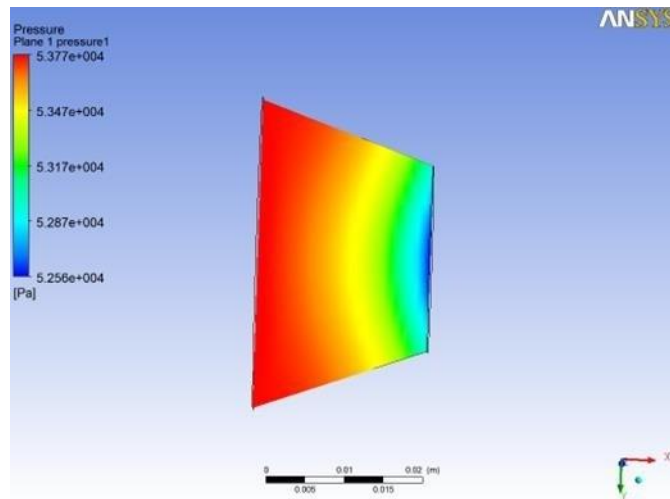


Figure 11: force difference for enture replica ( $\theta_c = 20$ ,  $\varnothing d = 11$ )

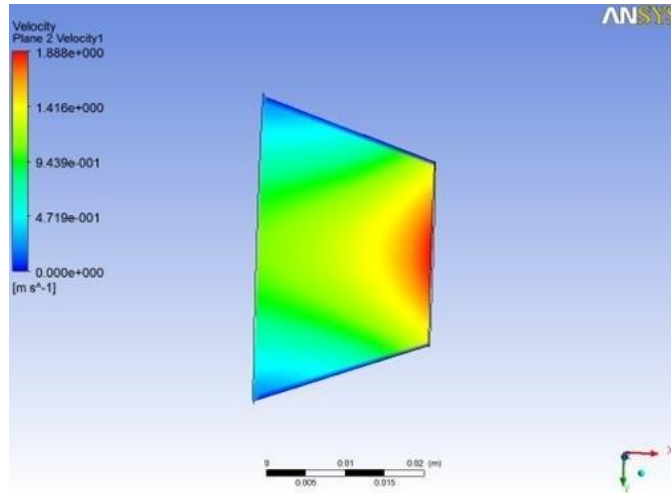


Figure 12: speed difference for entire replica ( $\theta_c = 20$ ,  $\text{Ø}d = 11$ )

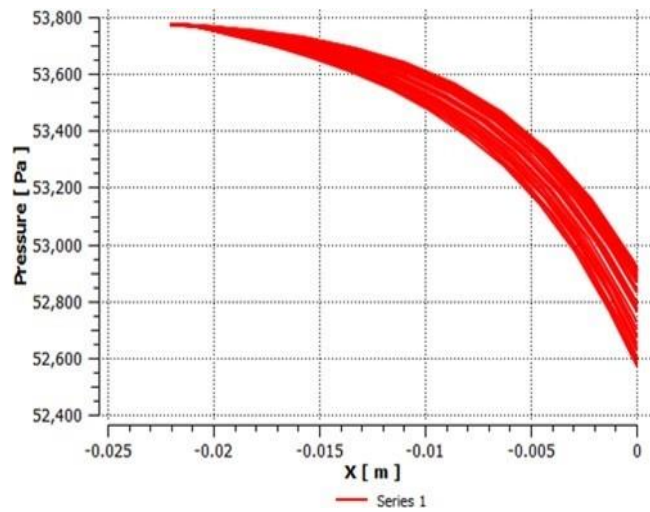


Figure 13: force difference plan for convergent part ( $\theta_c = 20$ ,  $\text{Ø}d = 11$ )

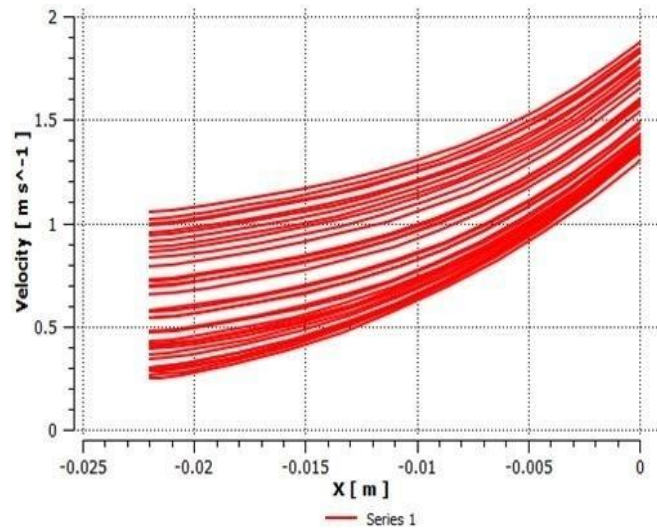


Figure 14: speed difference plan for convergent part ( $\theta_c = 20$ ,  $\text{Ø}d = 11$ )

### 3.3 Geometry type: Three

In the third arrangement of mathematical replicas having point  $\theta_c = 20$ ,  $\text{Ø}d = 11$  has been used to perform computational liquid active . The fall in force from 53660.54 Pa to 52420 Pa at the delta segment of venturi down the X course is as displayed in figure fourteen and figure sixteen. Speed variety is displayed in figure sixteen and figure seventeen with the shapes fluctuates from zero to 1.810 m/s.

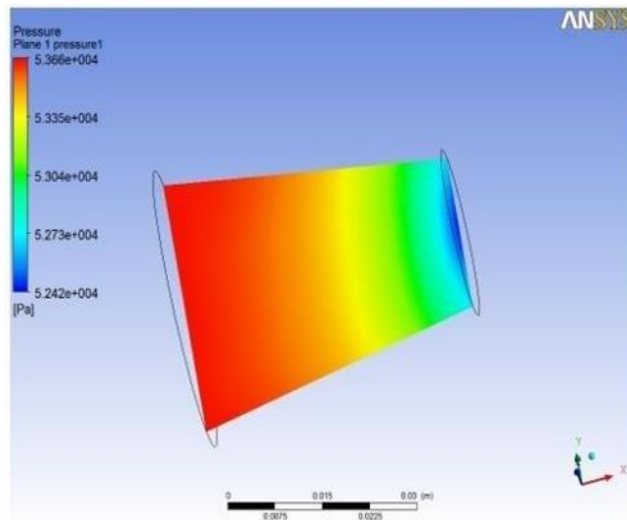
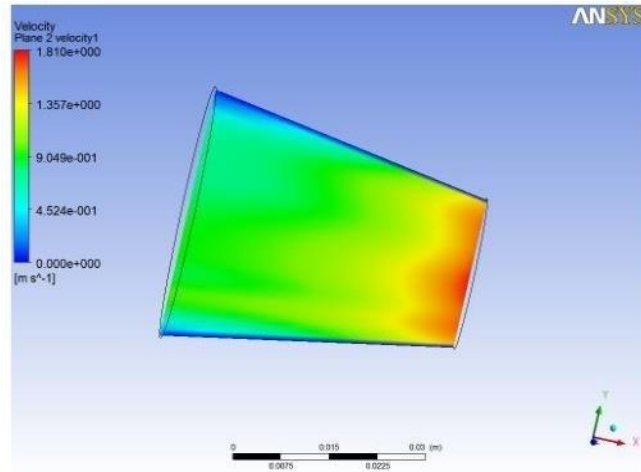
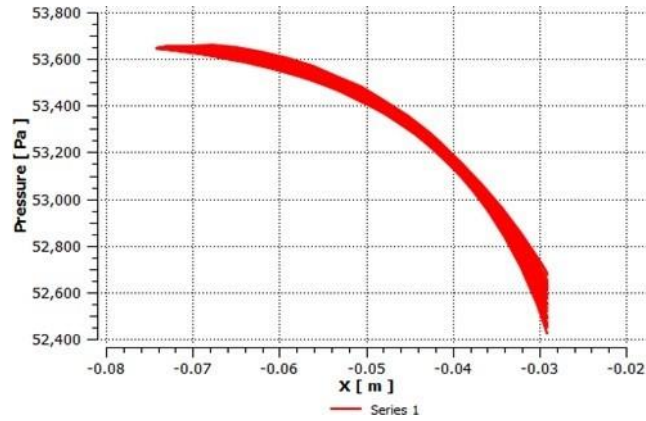


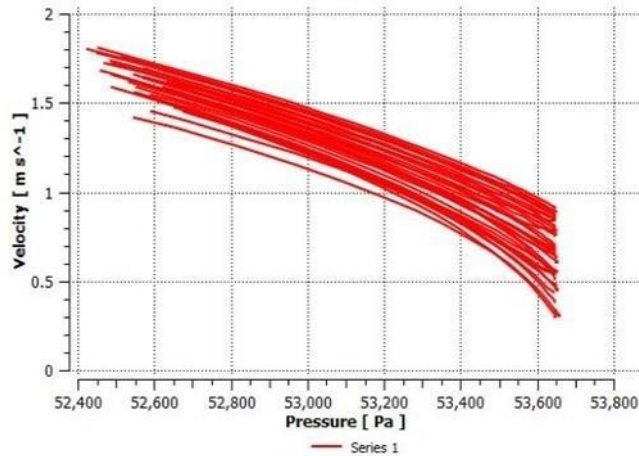
Figure 15: force difference for venturi replica ( $\theta_c = 21$ ,  $\text{Ø}d = 7$ )



**Figure 16:** speed difference for venturi replica ( $\theta_c = 21$ ,  $\text{Ø}d = 7$ )



**Figure 17:** force difference plan for convergent slice ( $\theta_c = 21$ ,  $\text{Ø}d = 7$ )



**Figure 18:** rate difference for venturi replica ( $\theta_c = 21$ ,  $\text{Ød} = 7$ )

Above executed examination with computational liquid elements has been done with the three diverse mathematical replicas having distinctive united and unique points as displayed figure two to figure four. Individual changes transversely the pressing factor and speed circulation have been read and assessed for liquid elements displaying and reproduction devices

### **3.4 Assessment of release coadjuvant (Cd) utilizing test and CFD investigation technique**

Hypothetical release for venturigaugage (Numerical calculation)

Distinction in manogauge level = x in m. of Hg Equivalent pressing factor drops (h) = x (13.6-1) m. of water h = 12.6 x meter of irrigate.  $Q_{th} = (0.002148\sqrt{h})$  for forty millimeter pipeline.

Genuine release for venturigaugage (Lab arrangement)

The space of gathering tank,

$$A = 0.6 \times 0.6 \text{ m}^2.$$

$$\text{Rise (R)} = 0.1 \text{ m}$$

Time taken= t sec.

The real release,

$Q_a = A.R/t$  Coadjuvant of release ( $C_d$ ) =  $Q_a/$

$Q_{th}$  Where,  $Q_a$  = Actual release for venturigaugage  $Q_{th}$  = Theoretical release for venturigaugage

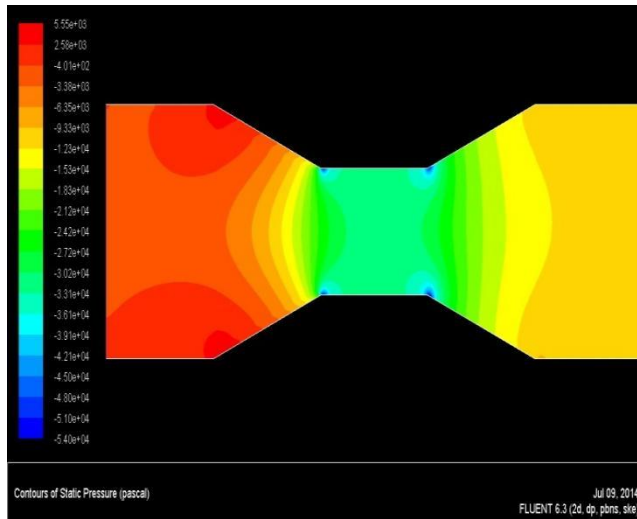
$h$  = Rise of water level in gathering tank

$x$  = Difference of pressing factor in manogaugage of liquid

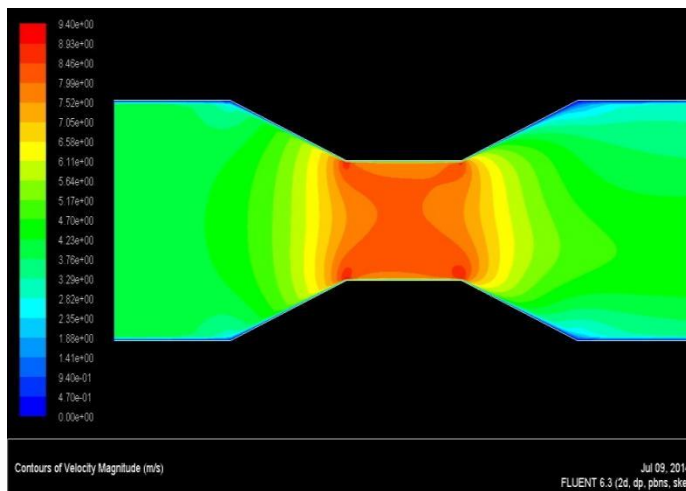
The worth of release coadjuvant ( $C_d$ ) determined utilizing mathematical calculation through a bunch of conditions for venturigaugage. Further estimations are completed for the diverse arrangement of concurrent points ( $\theta_c$ ) and dissimilar point ( $\theta_d$ ).

**Table 2:** modification in price of release coadjuvant ( $C_d$ ) for untried technique and CFD examination.

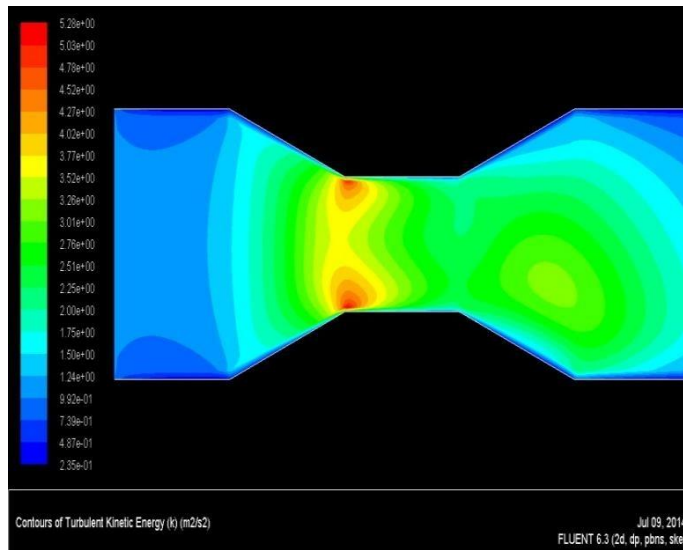
TABLE III: COMPARISON OF EXPERIMENTAL AND CFD ANALYSIS					
Type	Venturi Angles		Coadjuvant of discharge ( $C_d$ )		Change (%)
	$\theta_c$	$\theta_d$	Experimental Method	CFD analysis	
1.	21	9	0.9983	0.9443	5.40
2.	20	11	0.9079	0.8283	8.71
3.	21	7	0.8283	0.8887	6.80



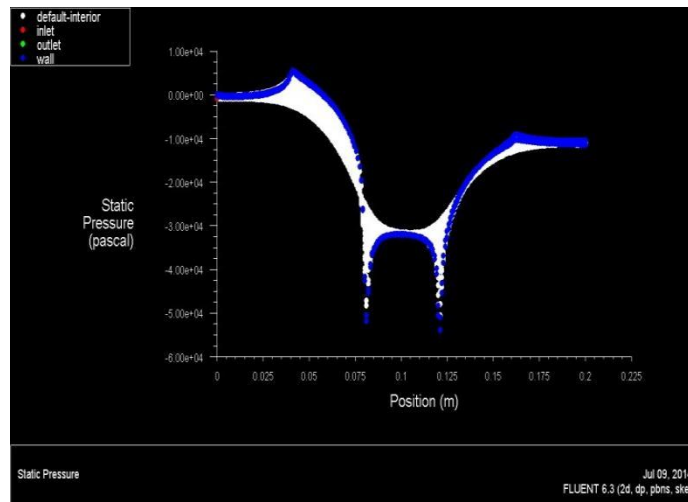
**Figure 19: Pressure contours**



**Figure 20: Velocity contours.**

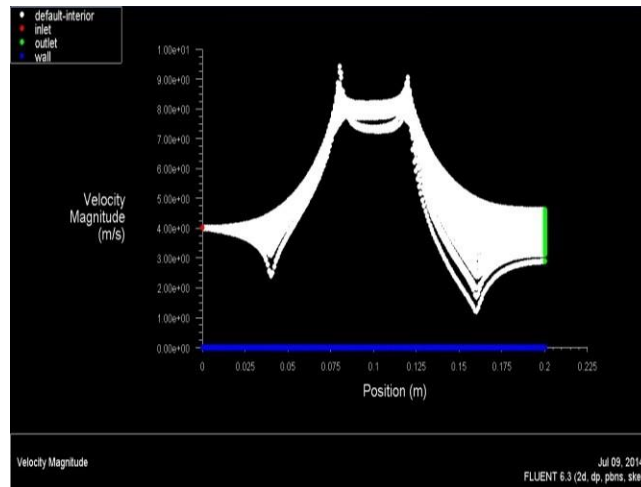


**Figure 21:** Turbulence contours.

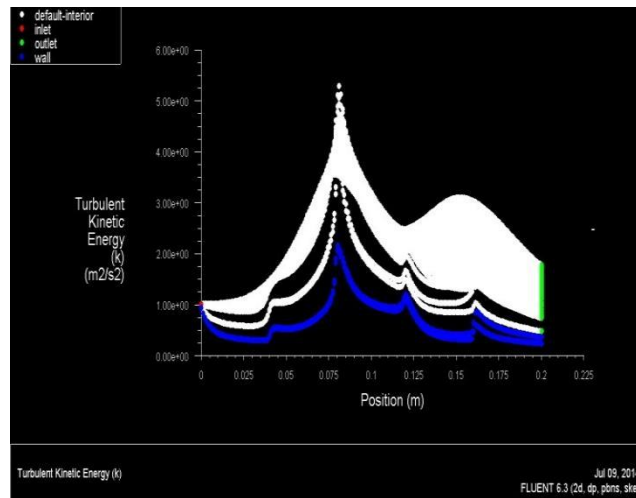


**Figure 22:** Static Pressure-Position





**Figure 23: Velocity-Position.**



**Figure 24: Turbulent-Position**

## CHAPTER 4 : CONCLUSIONS AND DISCUSSIONS

Various calculations of venturigaugue replicas are investigated and contrasted and the exploratory liquid lab arrangement results. In general estimation and reproductions are performed for the investigation of focalized ( $\theta_c$ ) and dissimilar points ( $\theta_d$ ) of venturi and their effect on the coadjuvant of release (Cd). The tested methodology incorporates analysis of various recreations by computational liquid elements advance, force dissemination plus speed circulations are inspected as form plots.

The venturi have beta proportion ( $\beta$ ) = zero point six, united point ( $\theta_c$ ) = twenty one and dissimilar point ( $\theta_d$ ) = 9 outcome with 5% of variety in the coadjuvant of release (Cd). While the ( $\theta_c$ ) = 20 and different point ( $\theta_d$ ) = 11 created variable outcomes as per the worth of coadjuvant of release (Cd). Here, the technique including test just as computational liquid elements (CFD) based demonstrated that the subsequent math replica of venturigaugue has moderate possibility when contrasted with the replica displayed with roughly 5% change in the coadjuvant of release (Cd).

In light of different mechanical utilizations of venturi, boundaries, for example, material, mass stream rate, real stream rate and drop in pressure and so forth which assumes a significant part to diminish the adjustment of level of coadjuvant of release (Cd).

In the examination, the course during Venturi pipe was dissected with SKE choppiness replica. The outcomes from the mathematical reenactment had been utilized to get the Cd qualities for every one of the examination. The Cd qualities acquired from reproduction for examination one, examination two and examination three were 0.97551, 0.98850 and 0.98902, separately, which arrived at the midpoint of to 0.984347. Experiment one brought about the most minimal Cd worth though Test three offered the greatest Cd benefit. The blunder among the exploratory and mathematical aftereffects of zero point nine three percent demonstrates the SKE disturbance replica concurred with the test information. The investigation additionally demonstrated that pressing factor has more computational effect contrasted with speed, and by understanding the

relationship between's pressing factor inclination and pressing factor, the focalized cone of the Venturi can be intended to work inside as far as possible at Venturi throat. From the examination and results got, it is exposed that the replica chose in the mathematical had been checked to be reasonable in the ensuing recreation in planning the Venturi pipe for the chat submission.

The impacts of the mathematical boundaries, for example, united cone point, unique cone point, beta proportion and throat length on pressure drop and streamlining were contemplated utilizing CFD examination. The degree of significance of the mathematical boundaries and their individual commitments in the pressing factor drop was controlled by utilizing investigation of fluctuation (ANOVA). In view of the outcomes acquired, the accompanying ends can be drawn: Analysis of difference recommends that the beta proportion is the main boundary for force fall having impact of ninety nine percent. The blend of ideal degrees of mathematical boundary is  $A1=17^\circ$ ,  $B1=seven\ degree$ ,  $C5=zero\ point\ seventy\ five$ ,  $D1=zero\ point\ zero\ zero\ seven\ millimeter$  and the worth of pressing factor fall at those boundaries.

The impacts of breadth, distance across proportion and CA on the presentation of a venturi gauge for damp chat gaugeing have been concentrated by demonstrating of the great pressing factor wet gas stream. The accompanying ends can be haggard from this examination: As the distance across builds, the impact of beta on the release coadjuvant diminishes. The OR esteems decline with expanding width proportion for a distance across of fifty millimeter and x more modest than that appears to be a superior decision for elevated pressing factor damp chat gaugeing. However, the CA doesn't influence OR qualities, it is prudent to pick a gauge with elevated release coadjuvant. Of the eight relationships tried, the HFM and the venturi connections executed superior compared to the hole connections.

The move through venturi gauge was mathematically recreated with water by consistent stream in k-epsilon plot. The significant perceptions made identified with the pressing factor, choppiness, speed forms and mass stream rate during the time spent stream. The exactness of results is within 5%. The speed and pressing factor distributions are described briefly and charts are plotted. To finish up, this assessment results show that FLUENT can be utilized with serious level of precision to picture the different forms of speed, pressing factor and disturbance can be

see unmistakably, the connection between the mass stream rate and pressing factor drop for each stream gauge is improved in the venturigauge.

There are numerous pipelines where streams should be precisely estimated. Gauges having an undeniable degree of precision and generally minimal expense a few the main boundaries when settling on the acquisition of a stream gauge. Most differential pressing factor stream gauges meet both of these necessities. A considerable lot of the most widely recognized stream gauges have a predetermined reach where the release coadjuvant might be viewed as consistent plus where the inferior finish is generally the base suggested Re figure that ought to be utilized with the predefined gauge. With the extra information on this investigation it will empower the client to all the more likely gauge the course during a tube over a more extensive scope of Reynolds information.

The examination finished in this investigation on release coadjuvants zeroed in on four unique kinds of stream gauges with changing beta proportions. The resultant release coadjuvants ought to just be utilized for comparable calculations to those utilized in the examination and not for those which change extraordinarily, but rather the outcomes ought to pursue a comparative direction. A total investigation on the impact of fluctuating beta proportions was not finished, so the consequences of this examination ought to just be practical as potential patterns to varying beta qualities.

The Venturi gauge was demonstrated utilizing two marginally various calculations to decide whether there was critical impact on the ensuing over the Re reach. It was tracked down that together of the informational collections pursued fundamentally the same as directions notwithstanding having various calculations. The stream gauge that had the illustrative joining cone, which makes less tempestuous misfortunes than the portioned uniting, had a somewhat bigger C all through the Re reach recreated. The beta worth tried for the two gauges was 0.661 for a 6.065-inch tube. In the investigation it was tracked down that the released coadjuvant.

The normal concentric hole protect was demonstrated utilizing four distinctive beta proportions and contrasted with Miller's information. The investigation inferred that the C versus Re for this stream gauge reacted dissimilar to the next three stream gauges, in light of the fact that the release coadjuvant isn't steady and shifts with the Re not at all like the other stream gauges researched. Despite the fact that there is no consistent C, there has been a lot of exploration on hole plates directed to decide the release coadjuvant qualities for Re more prominent than ten thousand. In the investigation for Reynolds information under ten thousand the release coadjuvants increment to a Re of around three hundred and afterward lessen, which is ascribed to an opening plate's impact on the speed outline. Since the most noteworthy speeds in a smooth line are situated in the middle, the little Re numbers have a bigger C in light of the fact that the majority of the speed related with the stream goes through the stream gauge without being as influenced by the opening plate at bigger Re. For Re information moving from hundreded is to one, the resultant C decreases relying upon the beta proportion of the gauge.

The V-cone stream gauge was demonstrated utilizing three distinctive beta qualities. It was resolved that as the beta qualities expanded from 0.66 to 0.82 that the comparing C qualities dropped from 0.803 to 0.731. For the consistent release coadjuvant the V-cone gauge deductions seemed, by all accounts, to be like that of the Venturi gauge with a change of under 1% for the Re scope of 30,000 to 50,000,000.

The block stream gauge was displayed utilizing two diverse beta qualities. Two diverse line sizes were utilized with a similar beta to decide whether there was any huge connection among release coadjuvants and stream gauge size. The outcomes demonstrated there to be moderately no contrast among the two replicas that had comparative beta qualities and diverse gulf widths.. As the segmental block expands comparative with the line measurement, it's anything but a bigger pressing factor differential for comparable streams and additional power is lost because of choppiness on the posterior of the block, hence diminishing the consistent C.

The CFD program FLUENT© was utilized to make various replicas with an end goal to comprehend patterns in the release coadjuvants for differential pressing factor stream gauges with fluctuating Reynolds numbers. The examination set up the release coadjuvant for Re

numbers going from one to five hundred thousand. For fierce stream systems irrigate was demonstrated as the streaming liquid, while for laminar stream runs weighty oil was displayed to make bigger viscosities bringing about more modest Re. Different replicas were created for every one of the stream gauges being dissected to decide impacts of line size and beta qualities on the release coadjuvant.

Clients should remember that since a couple of normal beta proportions were tried for every one of the gauges, there might be a variety of consequences when utilizing beta proportions establish exterior of the investigation variety. The Venturi, V-cone and block stream gauges all have relative consistent release coadjuvants for basic Reynolds numbers, yet with the extra data established in this investigation practically a wide range of streams can be resolved. The actual information range was little in contrast with the mathematical stream range for every one of the test reenactments. The precision of the mathematical outcomes ought to be most prominent at Reynolds quantities of under 2300, in light of the fact that choppiness replicas were not required in this locale accordingly expanding the exactness of the outcomes. The utilization of Computational Fluid energetic helps in the capacity to reproduce this examination while limiting individual mistakes. The information from this investigation exhibits that with conceivable release coadjuvants close 0.20 for a portion of the stream gauges that the iterative interaction be utilized to limit stream rate blunders.

Four distinct charts were created to introduce the consequences of the examination, with one diagram for every one of the stream gauges being considered. These diagrams can be utilized by perusers to decide how every gauge's exhibition might be described for tube streams for shifting viscosities of non-compressible liquids. The outcomes from this examination could be extended with prospect exploration of stream gauge release coadjuvants for extra differential delivering gauges.

One space exceptionally compelling is the chance of utilizing limit layers on the replica dividers while creating the replica cross section. Playing out this examination will assist with guaranteeing the exactness of utilizing the upgraded close divider treatment choice for the k-epsilon replica for tempestuous streams, as opposed to the standard divider treatment as utilized

in this investigation. An additional space of possible attention is analyzing examination over a broad scope of beta qualities to acquire a additional whole comprehension of release coadjuvant connections.

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